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COMPLETE SPECIFICATION.

Process for the Production of Distributable and Non-caking Fertilisers containing Calcium Nitrate.

We, Lonza Elektrizitätswerke und CHEMISOHE FABRIKEN AKTIENGESELL-SCHAFT, a Swiss Company, of Aeschen-vorstadt 72, Basle, Switzerland, and 5 Eur. Lüschen, of Eichensfrasse 25, and ERNST STIRNEMANN, of Gartenstrasse 105, both in Basle, Switzerland, both of Swiss Nationality, do hereby declare the nature of this invention and in what 10 manner the same is to be performed, to be particularly described and ascertained in and by the following statement:

This invention relates to a process for

the production of distributable and non-15 caking fertilisers containing calcium

nitrate.

The calcium nitrate commercially obtainable contains substantial amounts of water and has the property of 20 deliquescing rapidly in the air. Anhydrous calcium nitrate has always hitherto been obtained in a very fine mealy form and is considered, in general, as even more- hygroscopic than the ordinary more-hygroscopic than the ordinary
25 water-containing calcium nitrate. There
has, therefore, been proposed a method
for producing from unsuitable calcined
calcium nitrate a distributable product of
small hygroscopicity by innoculating the
30 calcined salt during its cooling with calcium nitrate containing water. The calcined calcium nitrate obtained in this way, on account of its high melting point, cannot be brought into the granular form advantageous for fertilising purposes by the usual process, for example by spray-

According to the present invention a readily distributable and non-caking pro-40 duct containing calcium nitrate especially suitable for fertilising is obtained by evaporating a calcium nitrate solution to a sandy-pasty consistency in which it contains about 90—95% of calcium nitrate (calculated as anhydrous calcium nitrate) and then converting the concentrated product without any substantial further concentration into granular form by mechanical disaggregation in bulk at 50 a temperature substantially above atmospheric of the order of 500 to 1000 C.

[Price 1/-]

of the sandy-pasty mass, of which the calcium nitrate at a concentration of about 90-95% consists, excludes fundamentally a spraying process, since the mass is not liquid enough for this purpose. .

By proceeding according to the present 60 invention it has been unexpectedly found that the apparently non coherent product obtained in this way, in spite of its sandy appearance, rapidly sets on cooling to very hard granules which are much more non-caking and distributable than any calcium nitrate fertilisers previously known in commerce. This is especially the case with the calcium nitrate fer-tilisers containing ammonium nitrate hitherto so very suceptible to caking. It has further been ascertained that the product obtained according to the present invention deliquesces much less readily in the air and that the granules themselves on taking up the same amount of mois-ture, retain the compact non-caking form which is not the case with ordinary calcium nitrate.

The evaporation process for preparation 80 of the 90—95 per cent. calcium nitrate product, preferably in its end phase, may be carried out in vacuo in a kneading machine adapted to be heated and

It has further been found that the material being treated can also be mixed before or during the cooling, with other fertilisers without detrimentally affecting the desired properties, indicated above, of the product to be obtained. The material which is being treated can be mixed, for example, with potash salts such as potassium nitrate, potassium chloride or potas-sium phosphate or mixtures of these. The preparation of mixtures of calcium nitrate with other salts is already known. Thus potassium or ammonium sulphate have been mixed with calcium nitrate the sulphates reacting with the calcium 100 nitrate to form insoluble calcium sulphate and the corresponding nitrates. It has also already been proposed to introduce spheric of the order of 50° to 100° C. burnt lime with the object of forming a

The process claimed of mechanical basic nitrate. The preparation of prodisaggregation at elevated temperatures ducts of this kind, in which the calcium

nitrate has been converted into other substances, does not come into consideration in the present case. Those salts which can give rise to undesirable reactions with calcium nitrate, are therefore to be added, after concentration of the calcium nitrate to 90-95% and before the cooling or rather, before or during the mechanical disaggregation at an elevated tem-10 perature.

It is already known to produce potashcontaining mixed fertilisers by introducing potash salts such as potassium nitrate into calcium nitrate solutions. It has been shown that to the usual calcium nitrate in the molten form not more than 20% of potassium nitrate can be added, as otherwise masses result which are extremely tough and difficult to work-20 with. In contradistinction to this the. calcium nitrate-containing fertilisers obtainable by the present process can have incorporated with them any desired amounts of other fertilising salts, for 25 example potash salts, in the manner indi-cated. The products thus obtained are quite crumbly, always set rapidly and are readily distributable and resistant to caking.

Examples. 1. 500 kg. of Ca(NO₂)₂.4H₂O are melted in a kneading machine adapted to be heated and the melt further evaporated under vacuum (down to 100 m.m. mercury) to a content of calcium nitrate of 94% while the temperature is raised to 90° C. The melt, at first thinly liquid, becomes rapidly thick and immediately afterwards changes over to a sandy-pasty

and mass. This is cooled to 80° C. and can easily be brought by mechanical disaggregation at 80° C. into a granular form.

The granules set very rapidly and become hard. The nitrogen content of the pro-

duct is 16.0%.

2. 440 kg. of acetylene mud which contains 27.1% CaO, 0.2% MgO. 1% Fe₂O, and Al₂O, and 1.25% SiO, is treated with so much 50% nitric acid (about 560 kg.)
that a neutral solution results. This is evaporated to a calcium nitrate content of about 75% then placed in a heated kneading machine and there further concertrated in vacuum to a content of over readily distributable and non-caking about 90% Ca(No₂). The temperature fertilizer containing calcium nitrate, subabout 90% Ca(No₂). The temperature fertilizer containing calcium nitrate, subwas increased to 110° C. thereby there quickly results a viscous product and shortly afterwards a sandy-pasty mass. 5. Fertilisers whenever prepared or This evaporated mass is then allowed to produced by the methods claimed. cool to 80° C. At this temperature it is Dated this 15th day of October, 1931. capable by mechanical disaggregation of being converted into the granular form.

Dated this 15th day of October, 1931.

W. P. THOMPSON & Co., being converted into the granular form. The product so obtained solidifies rapidly Chartered & Registered Patent Agents.

to compact, very hard granules. It contains 15.4% nitrogen.

3. 400 kg. of technical calcium nitrate-solution (obtained by dissolving limestone in nitric acid) which contains 7.8% of nitrogen is evaporated in a kneading device until a sandy-pasty mass results which contains 15.5% of nitrogen corresponding to about 90° Ca(NO₃)₂. To this is added at 110° C., 200 kg. of potassium nitrate and the whole thoroughly kneaded. The mass is then cooled to 75° C. and can be easily converted into the granular form by mechanical disaggregation at this temperature, which on further cooling yields well solidifying hard granules. The fertiliser has a content of 23% K₂O and 14.6% N.

Having now particularly described and

ascertained the nature of our said invention and in what manner the same is to be performed, we declare that what we claim is:-

1. Process for the preparation strewable, non-caking fertilisers containing calcium nitrate in which calcium nitrate solutions are evaporated to a sandy-pasty consistency in which they contain about 90-95 of calcium nitrate, and thereupon the thus obtained product, without any further substantial concentration, is converted into a granular form by mechanical disaggregation in bulk at a temperature substantially above atmospheric of the order of 50° to 100° C.

2. Process as claimed in claim 1 in 100 which the evaporation process for preparation of the 90-95 per cent. calcium nitrate product, preferably in its end phase, is carried out in vacuo in a knead-

ing machine.
3. Process as claimed in any of the preceding claims in which other fertilising salts, preferably potash salts such as potassium nitrate, potassium chloride or potassium phosphate or mixtures of these, 110 are added to the calcium nitrate, such salts as give rise to undesirable reactions with calcium nitrate being added after concentration of the original solution to

about 90—95% calcium nitrate content. 115
4. Process for the production of a

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